

IN THE SPECIFICATION:

Please replace the paragraph beginning on page 9, line 1 with the following amended paragraph:

The applicant put ~~her~~ research efforts into the development of an improved process for the production of very high quality lubricating oils and high quality middle distillates starting from hydrocarbon-containing feedstocks and preferably starting from distillates that are obtained from the direct distillation of crude or from conversion units such as FCC, coker or visbreaking, or obtained from units for extraction of aromatic compounds, or obtained from desulfurization or hydroconversion of RAT (atmospheric residues) and/or RSV (vacuum residues), or else the feedstock can be a deasphalting oil, or else a hydrocracking residue, for example, obtained from a hydrocracking stage, a vacuum distillate that has undergone a hydrorefining stage, and more generally bases for lubricating oils, or else polyalpha-olefins with a high pour point or any mixture of the feedstocks cited above, whereby the paraffins that are obtained from the Fischer-Tropsch process are excluded.

Please add the following subtitle beginning on page 57, before line 21 as follows:

Brief Description of Drawings

Please replace the paragraph beginning on page 58, line 10 with the following amended paragraph:

In this figure, before being introduced into zone (7), a large portion of ammonia and hydrogen sulfide H₂S are removed via pipe (6) from the feedstock to be hydroisomerized into in phase separator tank (5), via pipe (6), if the feedstock that enters via pipe 1 contains sulfur and nitrogen.

Please replace the paragraph beginning on page 58, line 13 with the following amended paragraph:

The effluent that is obtained from zone (7) is sent via a pipe (9) into a phase separator tank (10) for separation of the hydrogen that is extracted via a pipe (11); the effluent is then distilled at atmospheric pressure in column (12) from ~~where which~~ a light fraction that contains the compounds with at most 4 carbon atoms and those boiling below is ~~extracted withdrawn~~ at the top via pipe (13).

Please replace the paragraph beginning on page 58, line 19 with the following amended paragraph:

At the bottom of the column, there is obtained a fraction that contains ~~the~~ compounds ~~with having~~ a boiling point ~~that is~~ higher than at least 340°C ~~is obtained~~. This fraction is evacuated via pipe (17) to catalytic dewaxing zone (18).

Please replace the paragraph beginning on page 58, line 22 with the following amended paragraph:

~~Catalytic A catalytic~~ dewaxing zone (18) (comprising one or more reactors, one or more catalytic beds of one or more catalysts) also receives hydrogen via a pipe (19) for carrying out stage (b) of the process.

Please replace the paragraph beginning on page 59, line 1 with the following amended paragraph:

The effluent that is obtained and that exits via pipe (20) is separated in a distillation train that, in addition to phase separator tank (21) for separating the hydrogen via a pipe (22), comprises an atmospheric distillation column (23) and a vacuum distillation column (24) that treats the atmospheric distillation residue having an initial boiling point of higher than 340°C that is transferred via pipe (25), ~~residue with an initial boiling point of higher than 340°C~~.

Please replace the paragraph beginning on page 59, line 15 with the following amended paragraph:

To ~~declutter~~ simplify the figure, the hydrogen recycling ~~has not been~~ is not shown, whether at phase separating tank (10) toward hydrotreatment and/or the pretreatment stage and/or at tank phase separator (21) toward dewaxing and/or hydrofinishing.

Please replace the paragraph beginning on page 60, line 2 with the following amended paragraph:

In the same way as above, the references of reference numerals have the same meaning as in Figure 1 ~~have been preserved~~. In this embodiment, the effluent that is obtained from pretreatment-conversion stage (stage a) zone (7) undergoes in flask vessel (32), for example, a flash-separation of at least a portion of the light gases (hydrogen and hydrocarbon-containing compounds with at most 4 carbon atoms). The separated gases are extracted via pipe (33), and the residual effluent is sent via pipe (34) into catalytic dewaxing zone (18).